

Electrohydrodynamics of emulsion droplets

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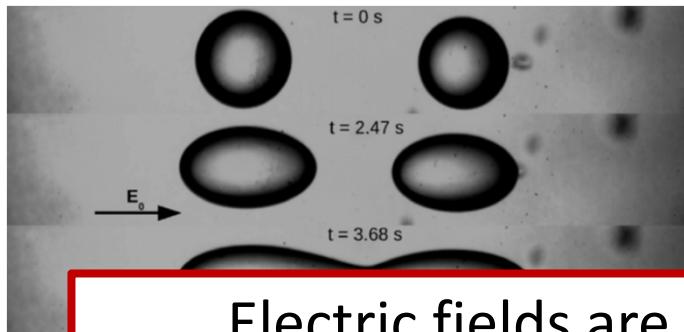
Carnegie Mellon University



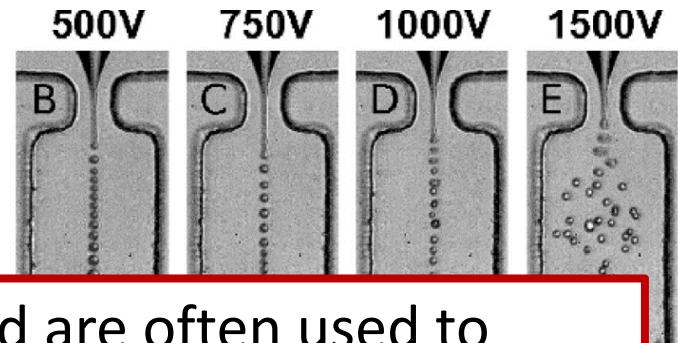
4th Edwards Symposium, Cambridge, September 4, 2019

Surfactant-laden fluid-fluid interfaces under electric fields

Electrocoalescence of Drops



Electroemulsification



Electric fields are efficient and are often used to manipulate fluid drops.

We started to think about the impact of particles, polymers and surfactants.



Kang et al. (2011)

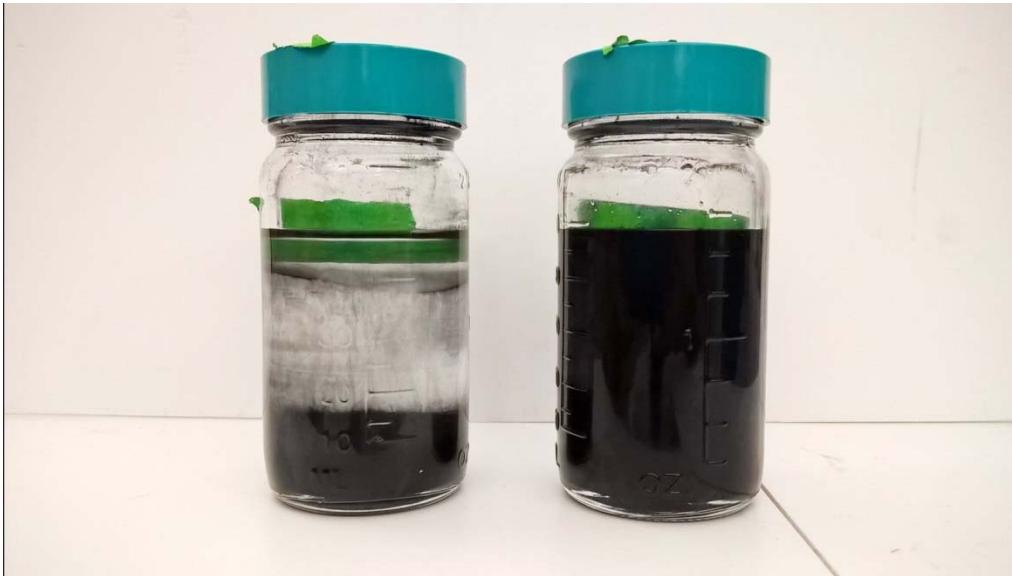
Suspension Loaded Drops



Squalane drop with 3.3 g/L carbon black particles + 2pph OLOA in silicone oil

What causes this breakup?

Drop: Carbon black particles suspended in squalane



Particles: Monarch 280 carbon black

Primary particle size: 30 nm

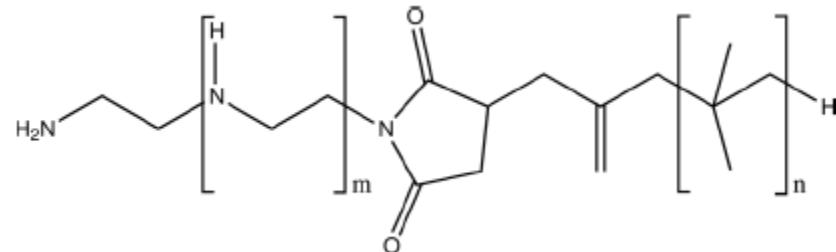
Primary aggregate size: 200 nm

3.3 g/L carbon black (fixed)

0.2% volume fraction

Surfactant: Polyisobutylene succinimide

OLOA 11000

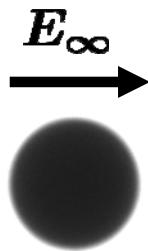


Smith and Eastoe (2012)

Surfactant concentration affects suspension stability



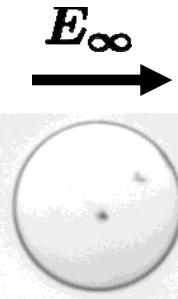
2 pph OLOA 30 pph OLOA
(unstable: steric) (stable: electrostatic)



Goal: How does suspension stability affect drop breakup?

Roadmap of experiments

Medium phase: Silicone oil (5000 cSt)

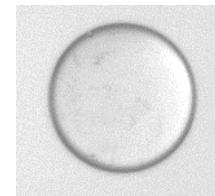


30 pph OLOA
(stable suspension)

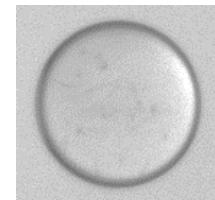


2 pph OLOA
(unstable suspension)

Pure squalane



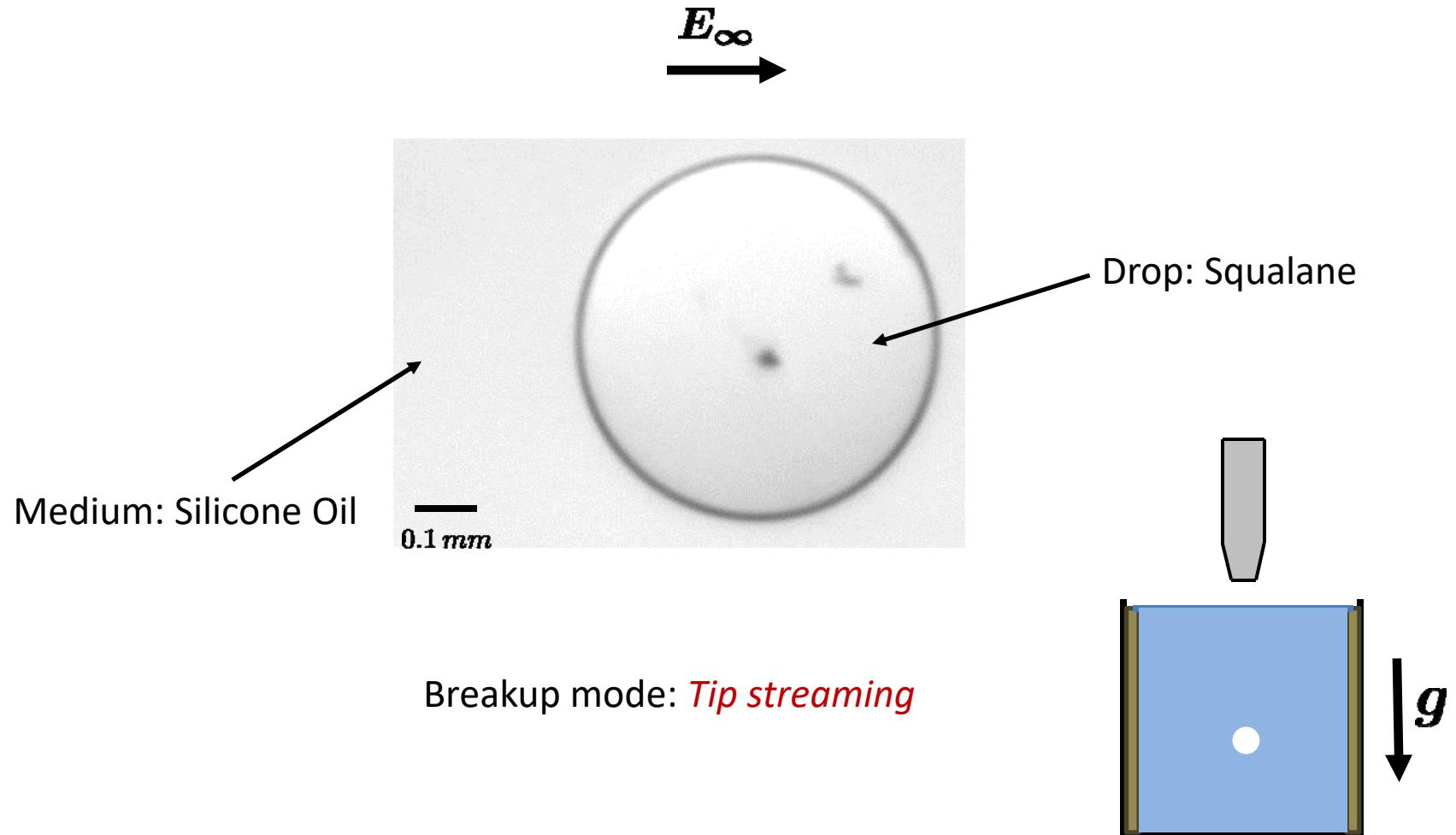
Equivalent OLOA (0.12 wt%)
No particles



Equivalent OLOA (0.008 wt%)
No particles

Pure squalane drop breaks via tip streaming

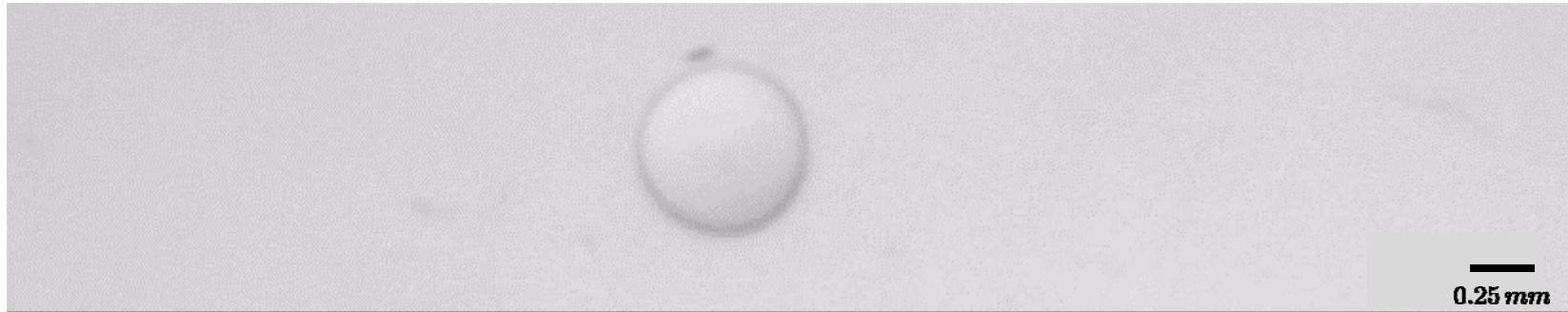
Drop of squalane in silicone oil – 7.6 kV/cm



Drop containing a stable colloidal suspension

$$E_{\infty} = 2.5 \text{ kV/cm}$$

→



*30 pph equivalent OLOA
No particles*

$$E_{\infty} = 2.5 \text{ kV/cm}$$

→



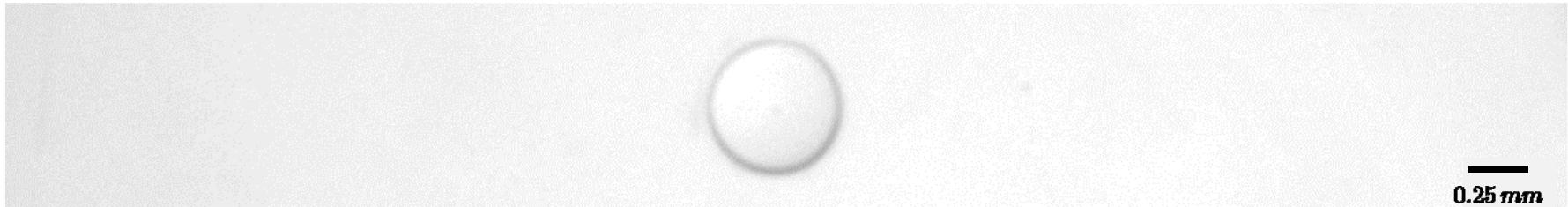
*30 pph OLOA
(stable)*

Breakup mode: *End pinching*

Particles do not qualitatively change breakup mode

Non-axisymmetric breakup at larger field

$$E_{\infty} = 5.3 \text{ kV/cm}$$

30 pph equivalent OLOA
No particles

$$E_{\infty} = 5.3 \text{ kV/cm}$$



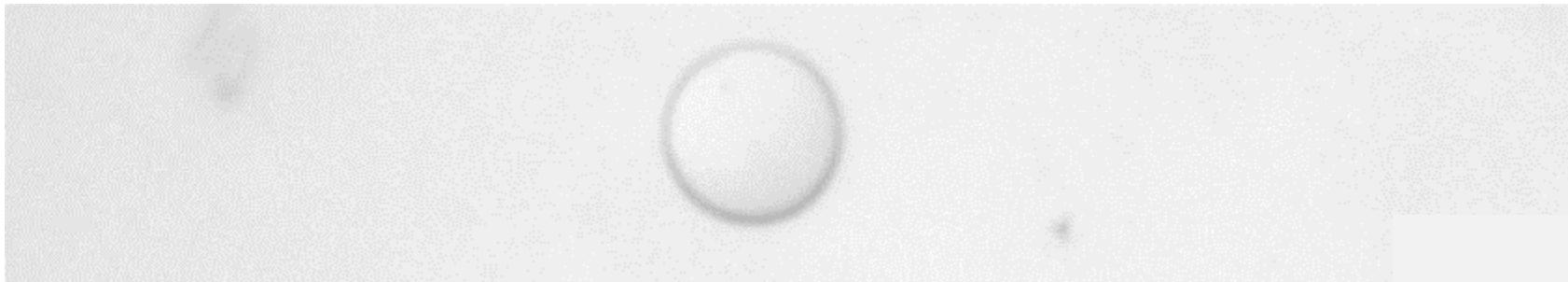

30 pph OLOA
(stable)

Breakup mode: *Charged lobe disintegration*

Again, particles do not qualitatively change breakup mode

Drop containing an unstable colloidal suspension

$$E_{\infty} = 2.5 \text{ kV/cm}$$



2 pph equivalent OLOA
No particles

Breakup mode: *End pinching*

$$E_{\infty} = 2.5 \text{ kV/cm}$$



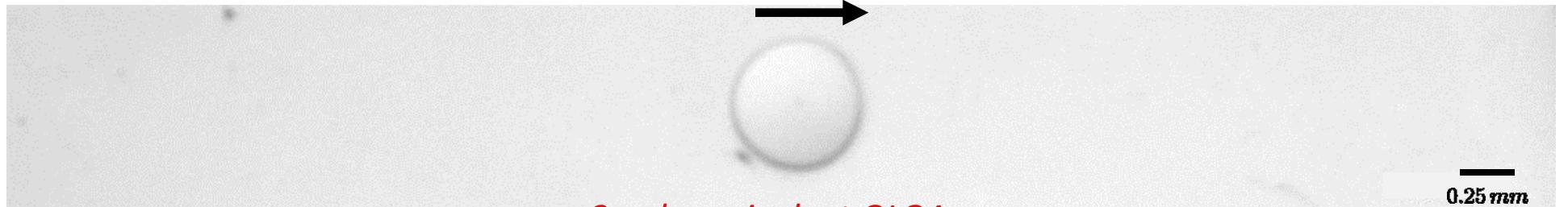
2 pph OLOA
(unstable)

Non homogeneous breakup

Particles do qualitatively change breakup mode

Unstable suspension at larger field

$$E_\infty = 5.3 \text{ kV/cm}$$

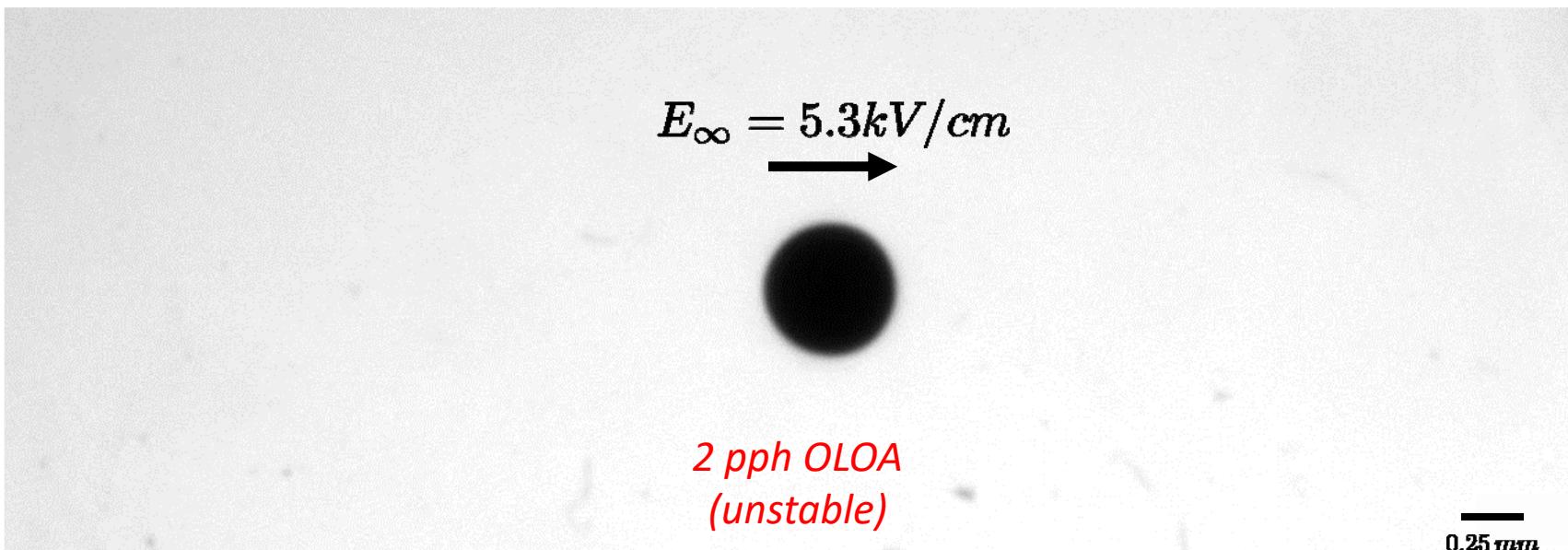


2 pph equivalent OLOA

No particles

Breakup mode: *End pinching*

$$E_\infty = 5.3 \text{ kV/cm}$$

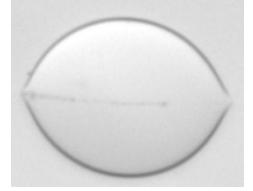
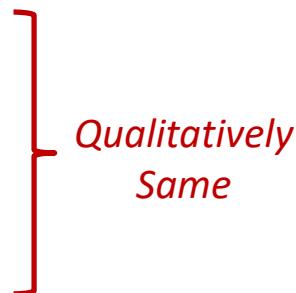
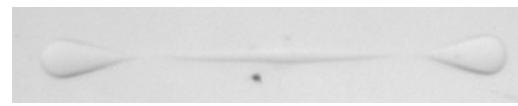
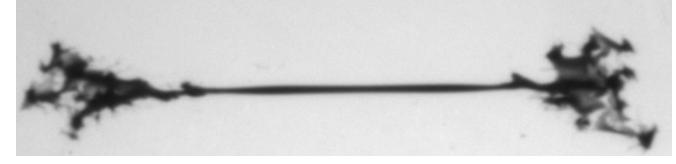


2 pph OLOA

(unstable)

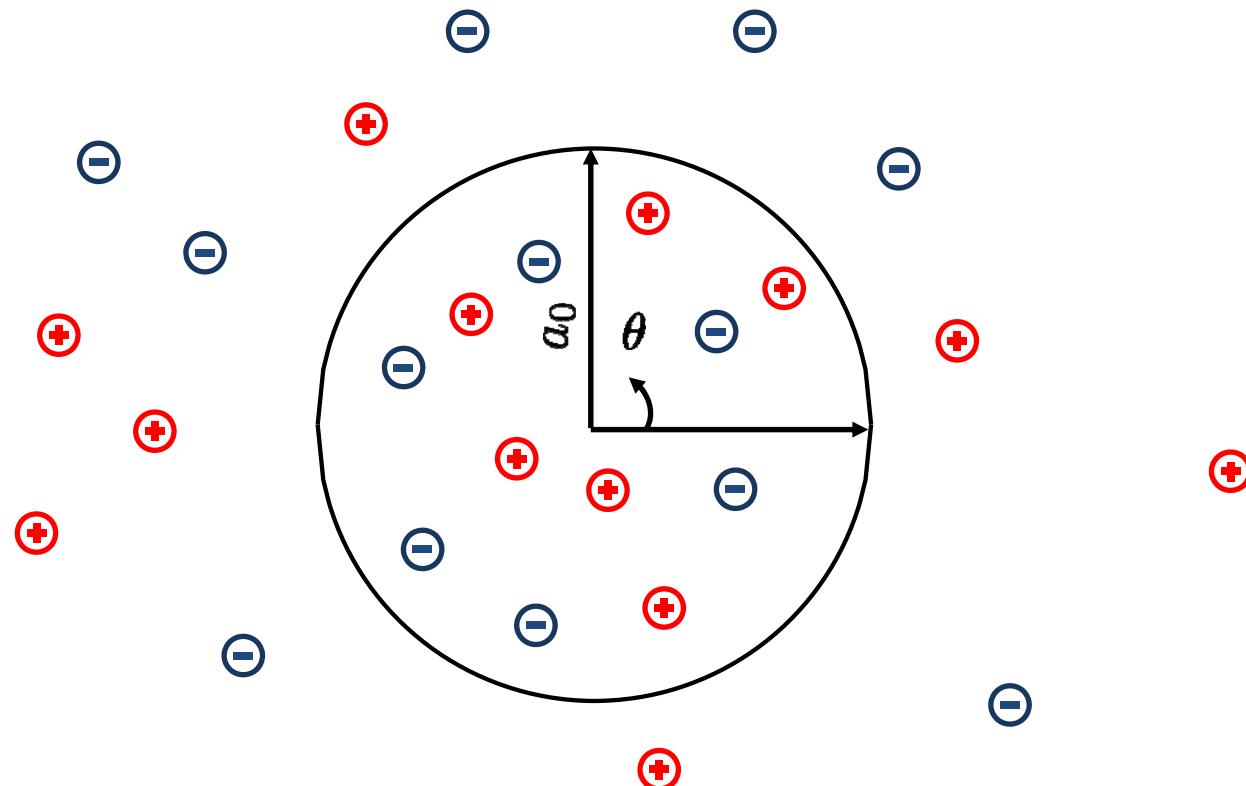
Unstable suspension again yields non homogeneous breakup

Summary of experiments

	2.5 kV/cm	5.3 kV/cm	7.6 kV/cm
Pure squalane	No breakup	No breakup	
30 pph OLOA	 End pinching	 Charged lobe disintegration	 Tip streaming
30 pph (Stable)	 End pinching	 Charged lobe disintegration	
2 pph OLOA	 End pinching	 End pinching	
2 pph (Unstable)	 Non homogeneous	 Non homogeneous	

Leaky Dielectric Model

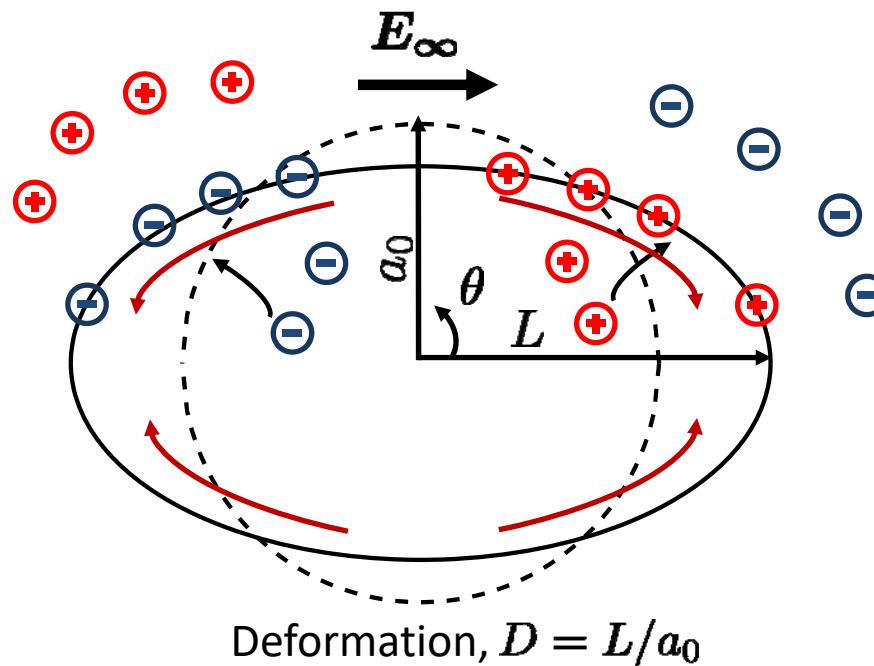
- Small electrical conductivity (impurity); bulk is electroneutral



An undeformed drop

Leaky Dielectric Model

- Interface is charged under an electric field
- Electric traction acts along the interface and deforms the drop
- Drop breaks above a critical field



Final state of the drop = $f(M = \frac{\mu_i}{\mu_o}, S = \frac{\varepsilon_i}{\varepsilon_o}, R = \frac{\sigma_o}{\sigma_i}, Ca_E = \frac{a_0 \varepsilon_o E_\infty^2}{\gamma}, Re_E = \frac{\varepsilon_o^2 E_\infty^2}{\mu_o \sigma_o})$

Boundary Integral Computations to predict drop deformation

14
Taylor, 1966

Computing nonlinear deformation

Boundary Integral Method: Convert differential equations in the domain to integral equations along the boundary

Electric Field

$$\nabla^2 \phi = 0$$

Jump in Normal Field

$$\frac{1}{S} E_{n,o} - E_{n,i} = \frac{1}{S} q$$

Interfacial Charge Transport

$$\frac{1}{R} E_{n,i} - E_{n,o} = \frac{Re_E}{Ca_E} \frac{\partial q}{\partial t} + Re_E \nabla_s \cdot (\mathbf{u} q)$$

Fluid Flow

$$\nabla^2 \mathbf{u} = \nabla p \quad \nabla \cdot \mathbf{u} = 0$$

Computing nonlinear deformation

Boundary Integral Method: Convert differential equations in the domain to integral equations along the boundary

Electric Field

$$\mathbf{E}^\infty \cdot \mathbf{n} + \frac{1}{4\pi} \oint_A \frac{\mathbf{r} \cdot \mathbf{n}}{r^3} \Delta E_n dA = \frac{1}{2}(E_{n,o} + E_{n,i})$$

Jump in Normal Field

$$\frac{1}{S} E_{n,o} - E_{n,i} = \frac{1}{S} q$$

Interfacial Charge Transport

$$\frac{1}{R} E_{n,i} - E_{n,o} = \frac{Re_E}{Ca_E} \frac{\partial q}{\partial t} + Re_E \nabla_s \cdot (\mathbf{u} q)$$

Fluid Flow

$$\mathbf{u}_o = -\frac{1}{4\pi(M+1)} \oint_A \Delta f \cdot \mathbf{J} dA + \frac{3}{2\pi} \frac{M-1}{M+1} \oint_A \mathbf{u}_o \cdot \mathbf{K} \cdot \mathbf{n} dA$$

A = drop surface

Nonlinear deformation with insoluble surfactant

Boundary Integral Method: Convert differential equations in the domain to integral equations along the boundary

Electric Field

$$\mathbf{E}^\infty \cdot \mathbf{n} + \frac{1}{4\pi} \oint_A \frac{\mathbf{r} \cdot \mathbf{n}}{r^3} \Delta E_n dA = \frac{1}{2}(E_{n,o} + E_{n,i})$$

Jump in Normal Field

$$\frac{1}{S} E_{n,o} - E_{n,i} = \frac{1}{S} q$$

Interfacial Charge Transport

$$\frac{1}{R} E_{n,i} - E_{n,o} = \frac{Re_E}{Ca_E} \frac{\partial q}{\partial t} + Re_E \nabla_s \cdot (\mathbf{u} q)$$

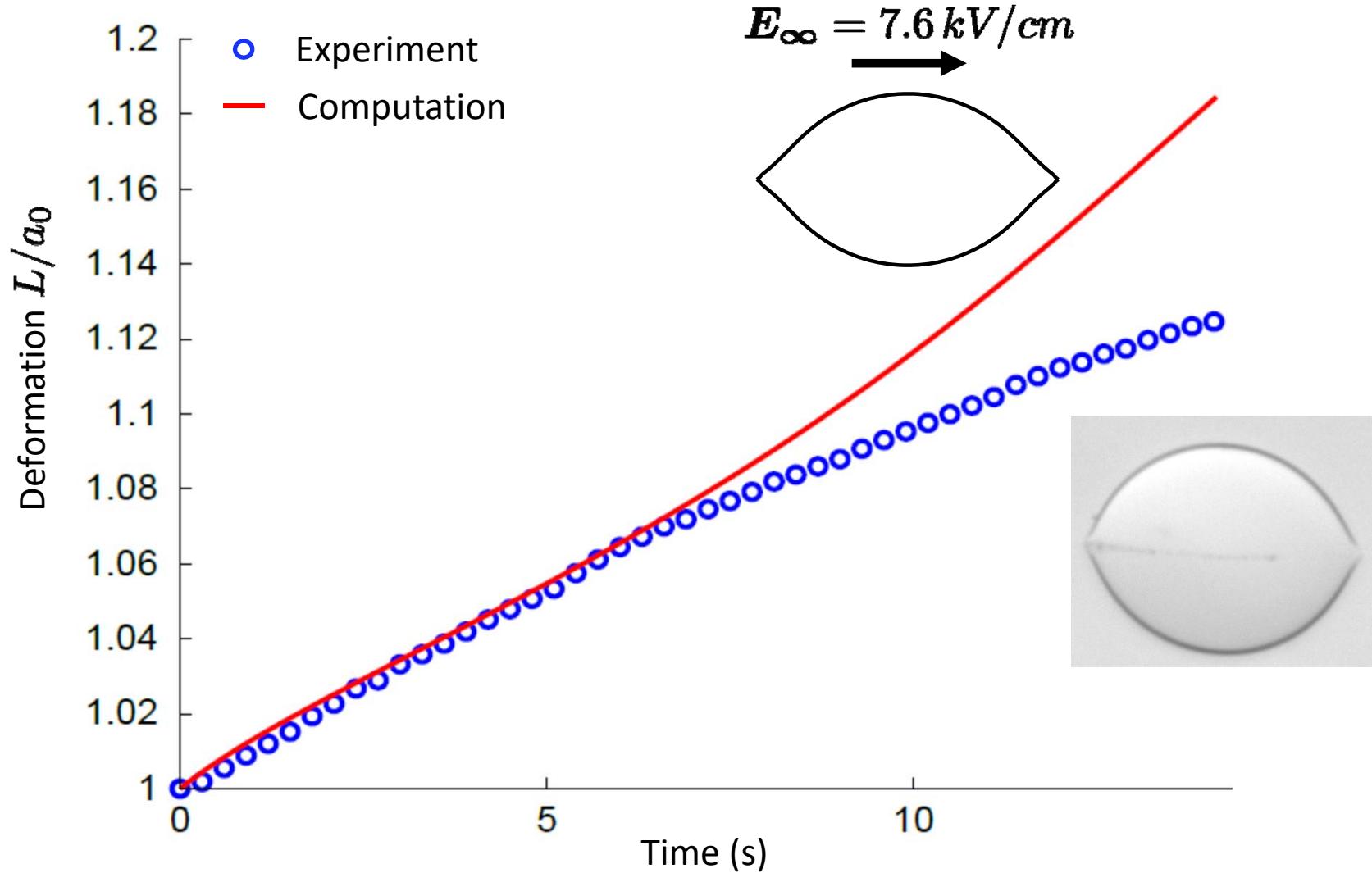
Fluid Flow

$$\mathbf{u}_o = -\frac{1}{4\pi(M+1)} \oint_A \Delta f \cdot \mathbf{J} dA + \frac{3}{2\pi} \frac{M-1}{M+1} \oint_A \mathbf{u}_o \cdot \mathbf{K} \cdot \mathbf{n} dA$$

Surfactant Transport

$$\frac{1}{Ca_E} \frac{\partial \Gamma}{\partial t} + \nabla_s \cdot (\mathbf{u}_s \Gamma) + (\mathbf{u}_s \cdot \hat{\mathbf{n}}) \kappa \Gamma - \frac{1}{Pe_s} \nabla_s^2 \Gamma = 0$$

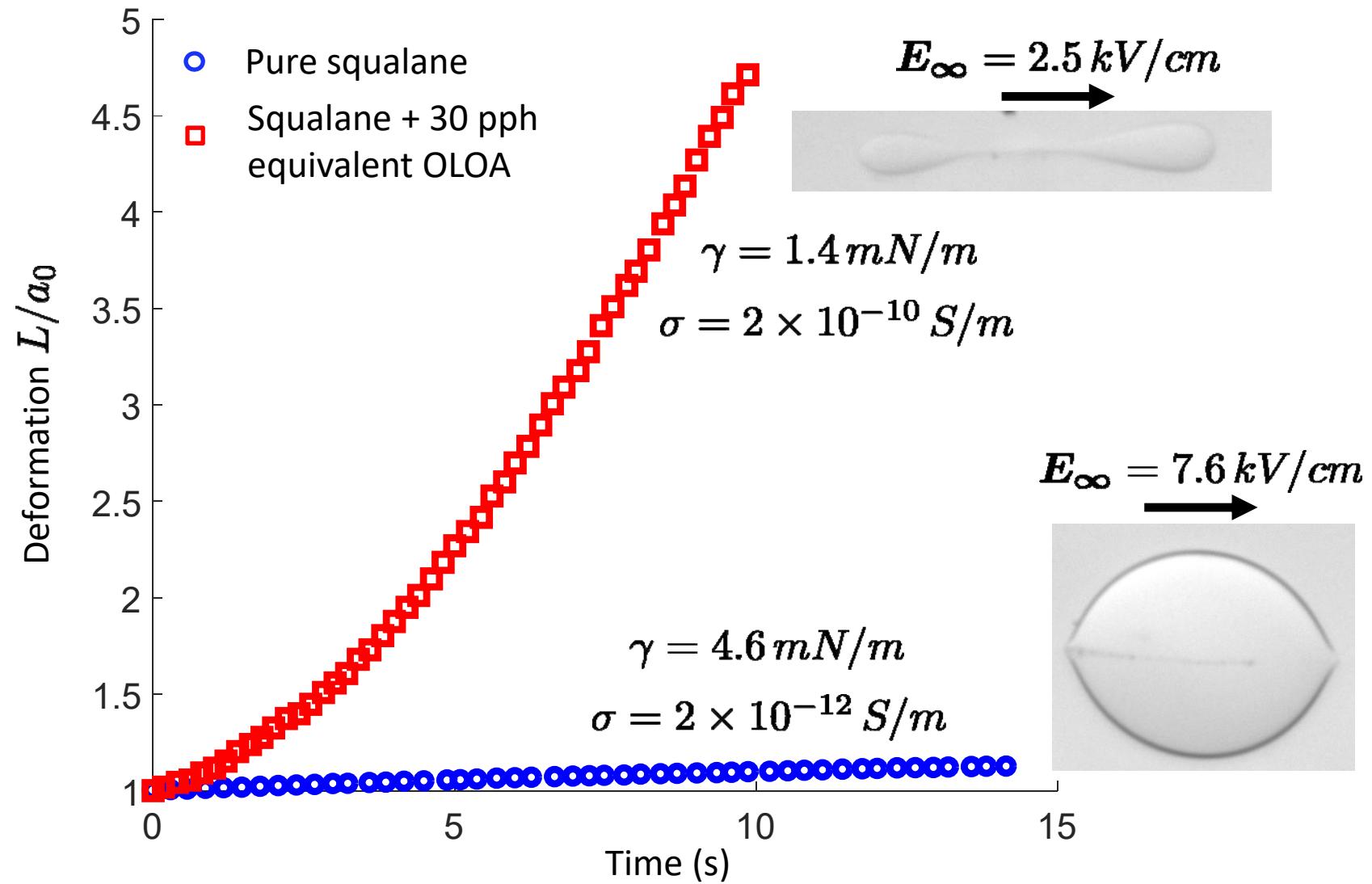
Pure Squalane Drop



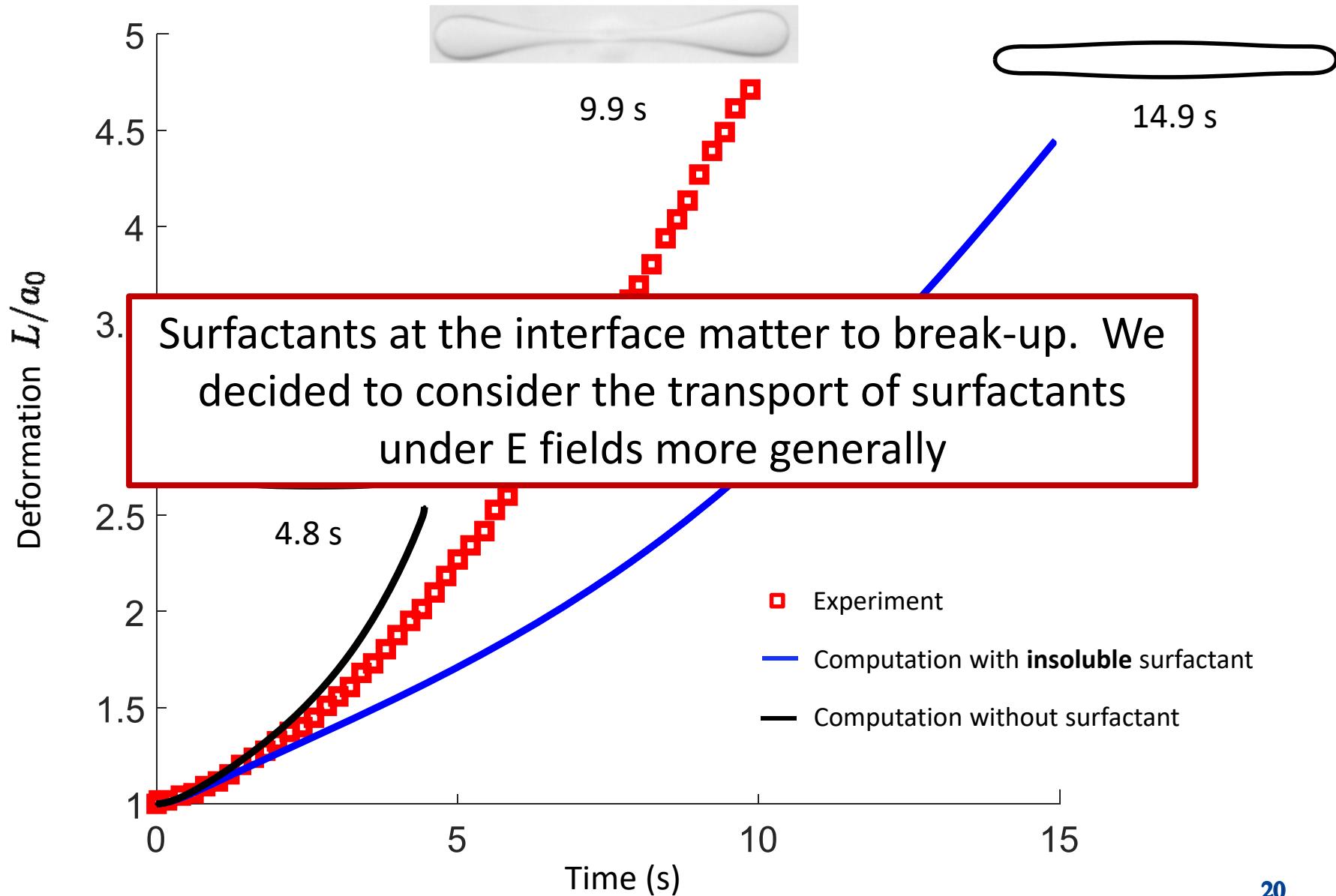
Computations capture experimentally observed breakup mode

Lanauze et al., Soft Matter, 2018

Surfactant addition changes conductivity and interfacial tension

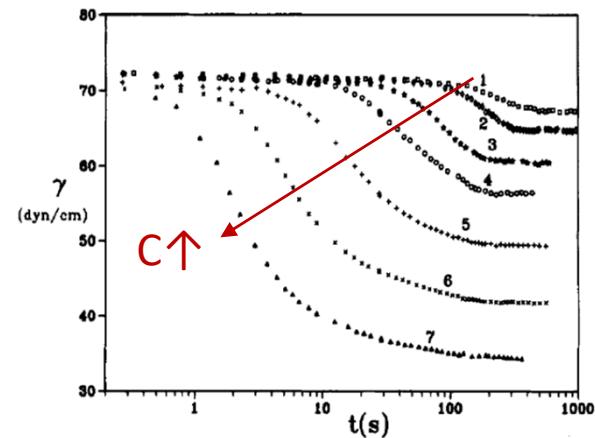


Marangoni stresses change breakup mode



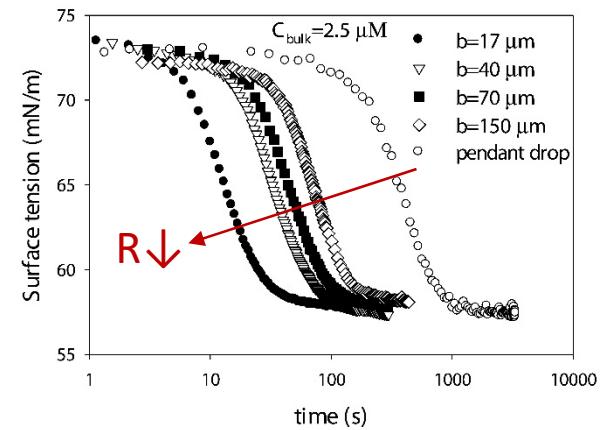
Do electric fields affect surfactant transport?

Bulk concentration



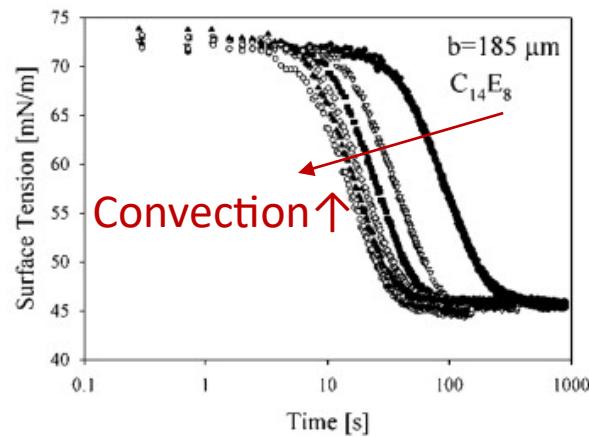
Lin *et al.* (1995)

Interface radius



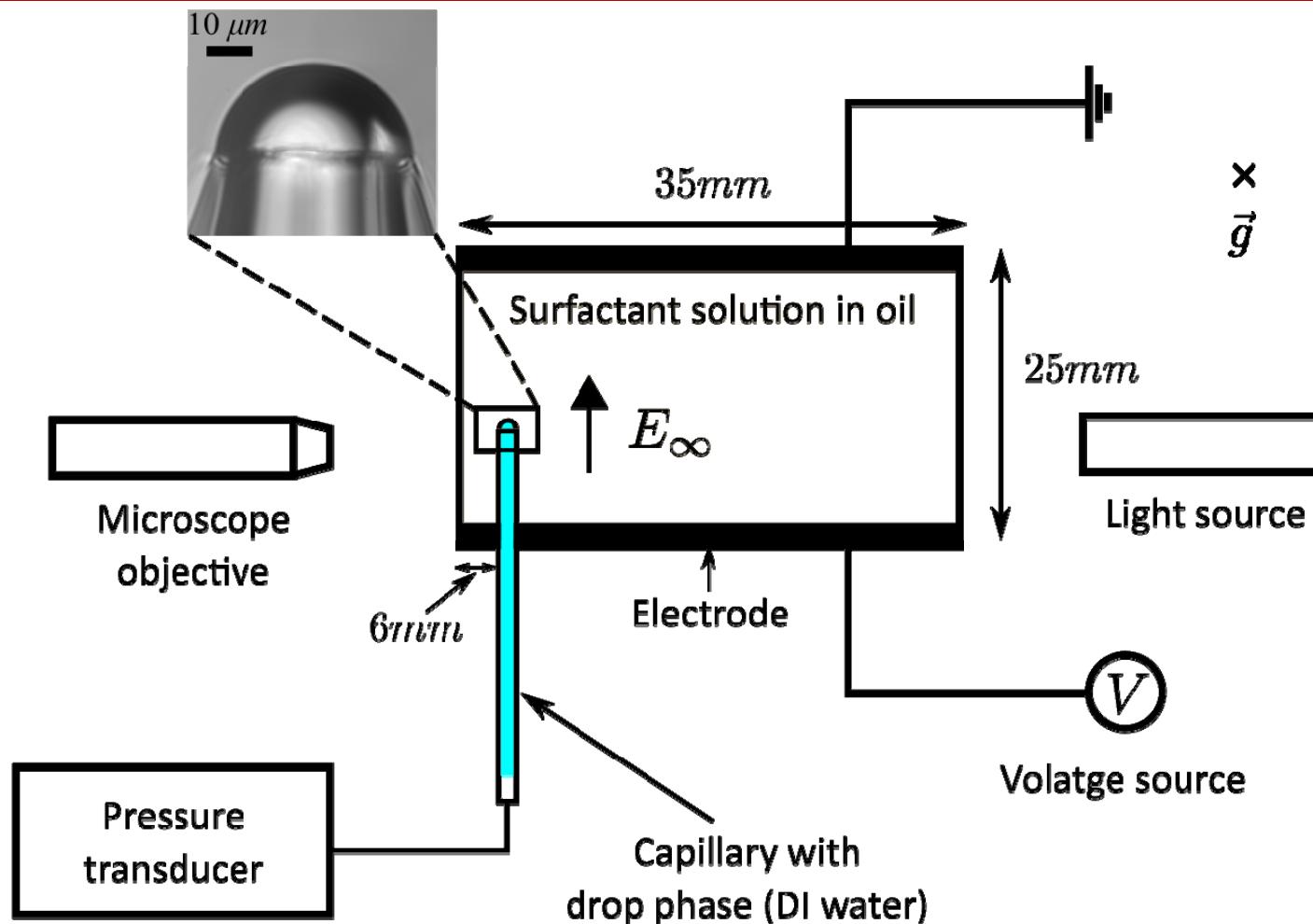
Alvarez *et al.* (2010)

Bulk convection



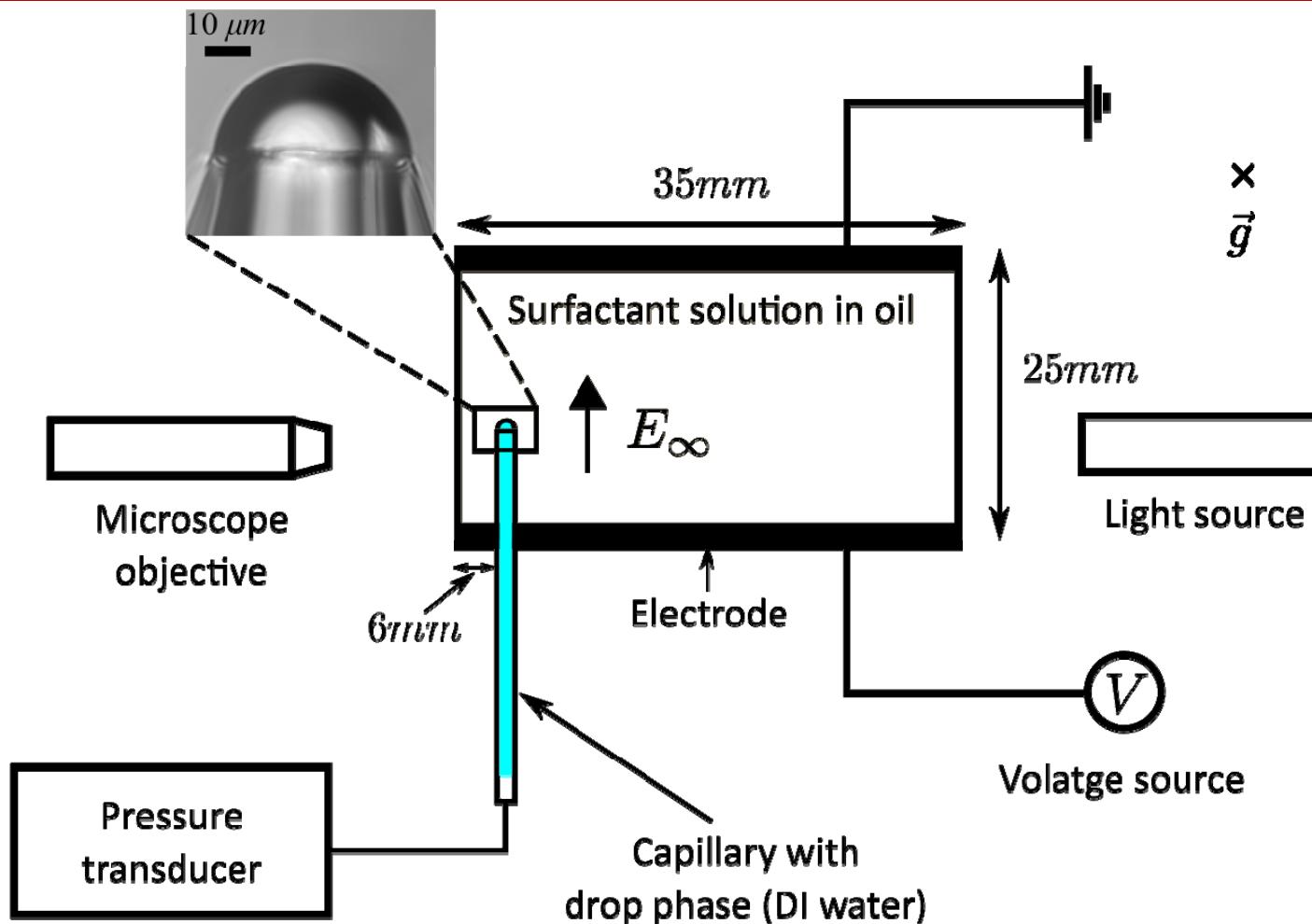
Alvarez *et al.* (2012)

Electrified micro-tensiometer to measure interfacial tension



$$\Delta P = \frac{2\gamma}{R} + \Delta T'_E$$

Electrified micro-tensiometer to measure interfacial tension



$$Ca_E = \frac{R\varepsilon_o E_\infty^2}{\gamma} < 10^{-4}$$

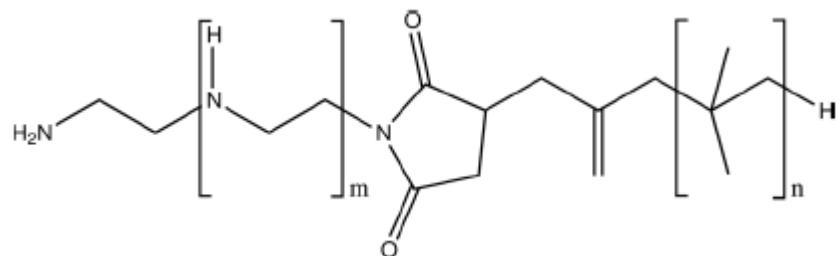
$$\frac{R\Delta P}{\gamma} = 2 + Ca_E \Delta T_E$$

Reservoir phase: Surfactant dispersed in oil

Material 1

Surfactant: Polyisobutylene succinimide

OLOA 11000

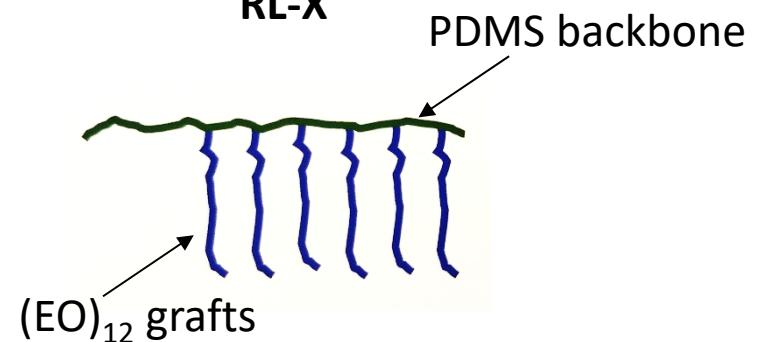


Oil: Isopar-M (alkane mixture)

Material 2

Surfactant: Polydimethylsiloxane (PDMS)
based rake surfactant

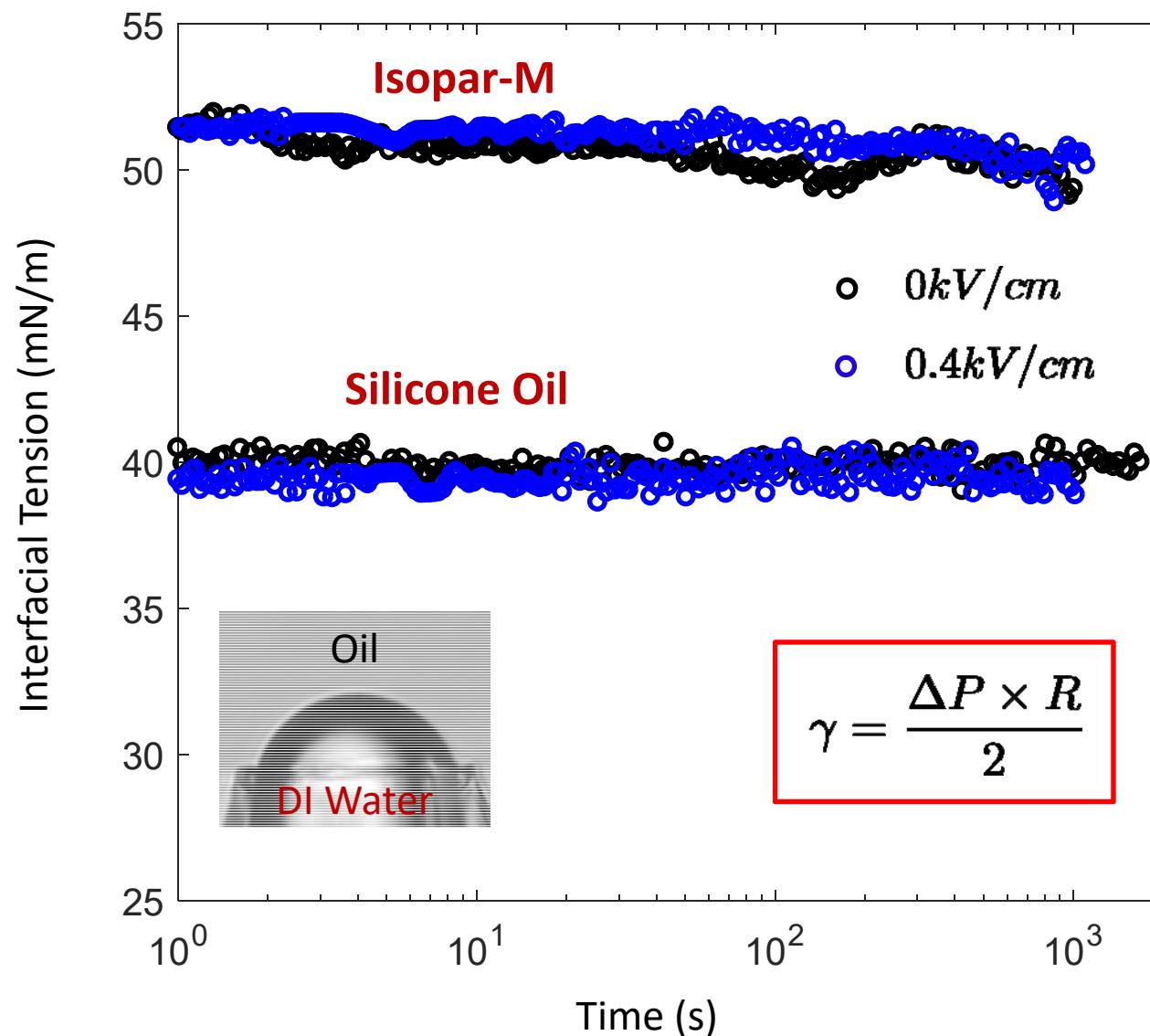
RL-X



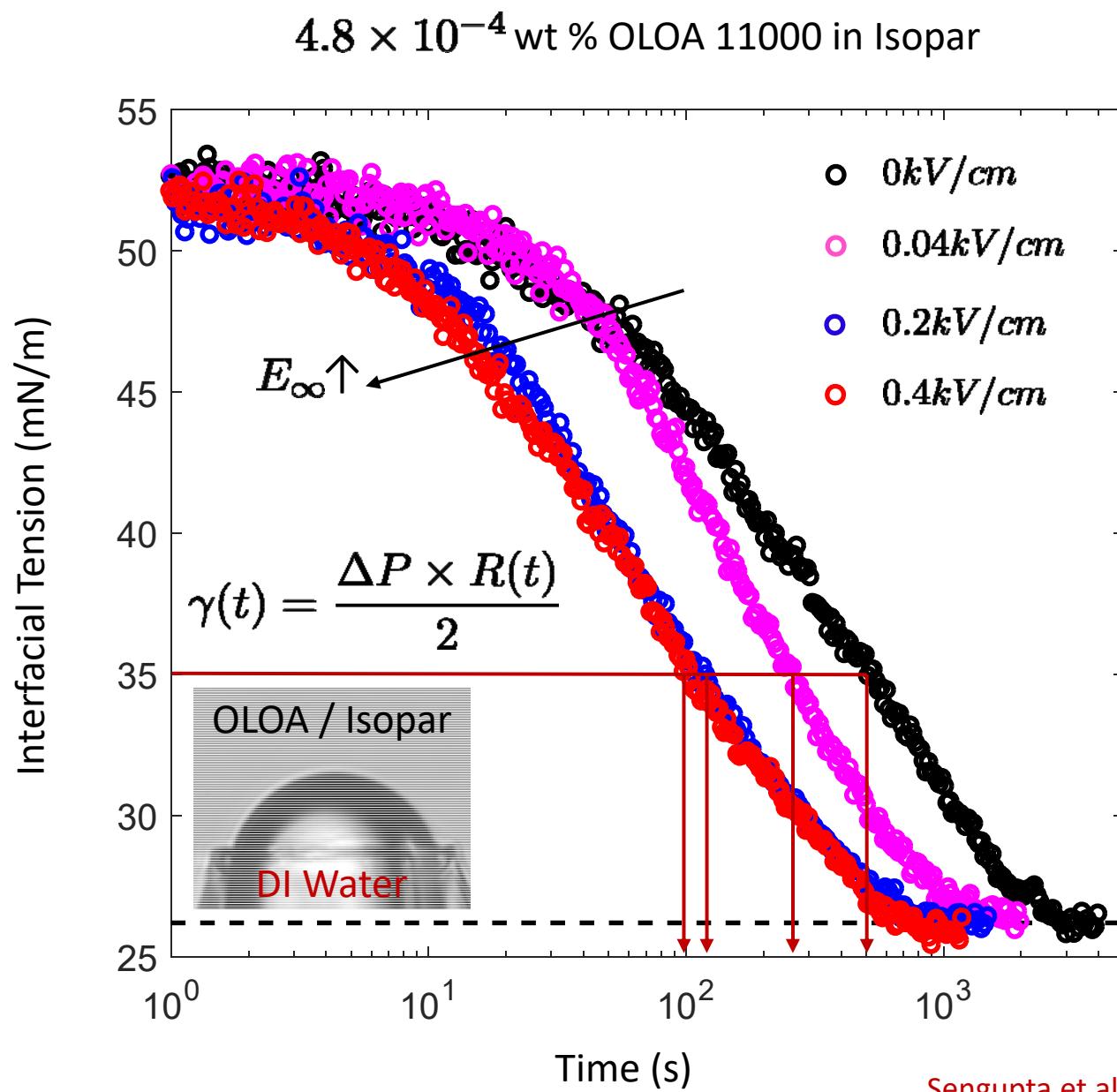
Oil: Isopar-M (alkane mixture)

The surfactants ***do not dissociate*** in oil

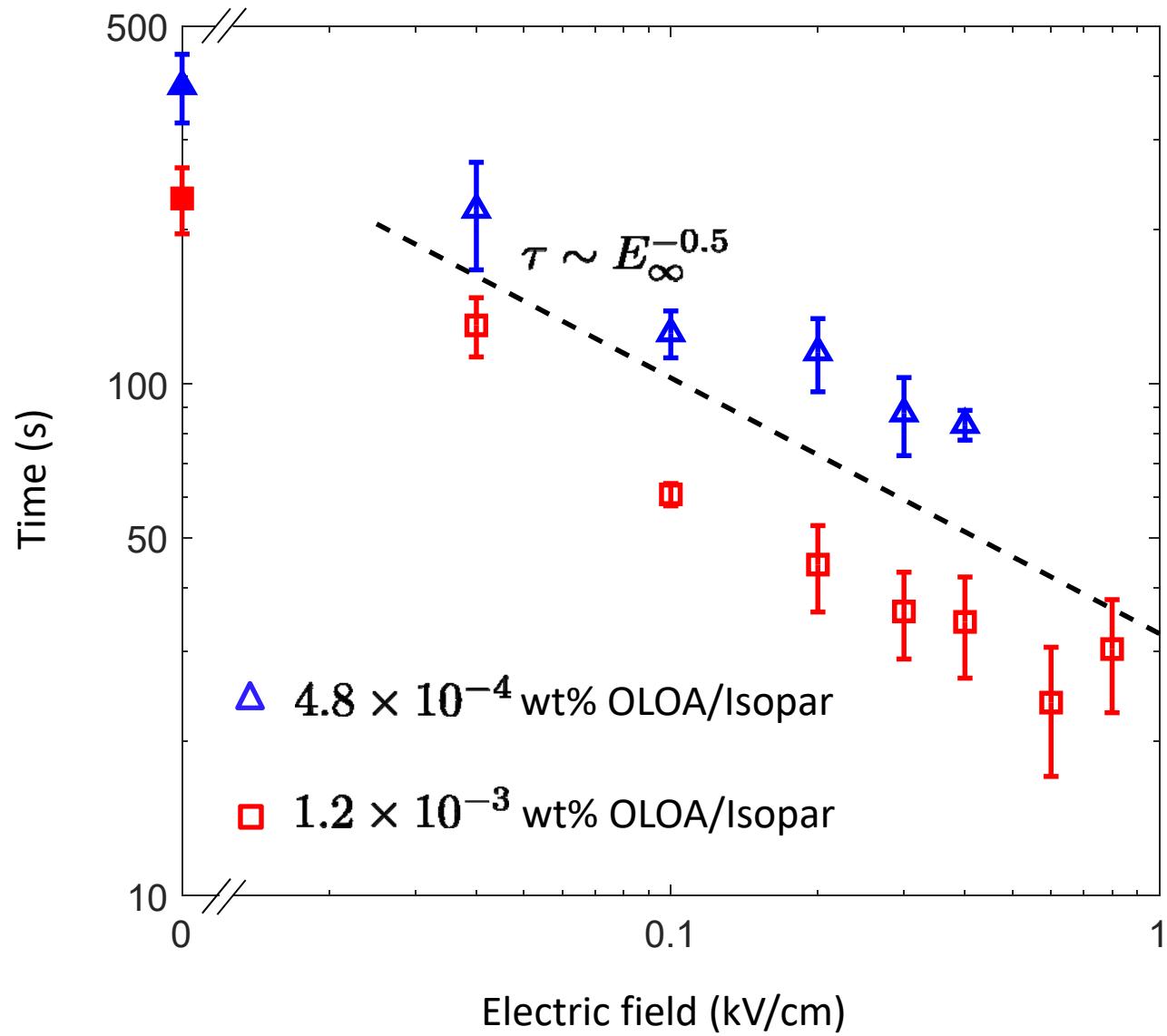
Electric field does not change interfacial tension of pure oil-water



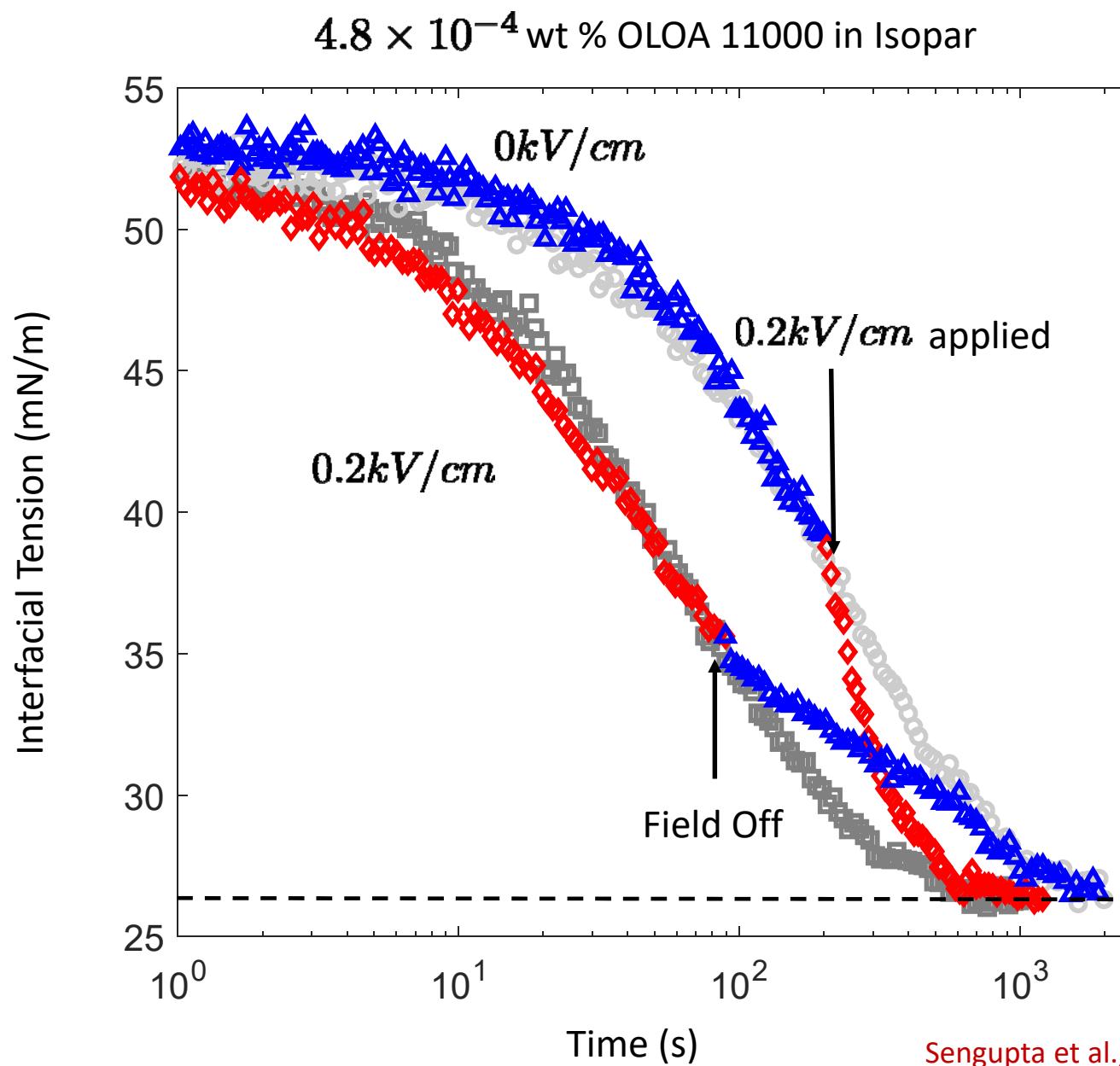
Transport of OLOA is enhanced under electric field



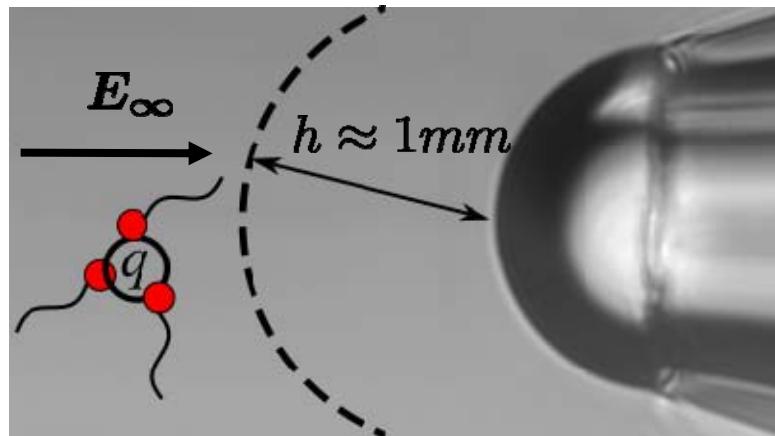
Time to reach specific interfacial tension decreases with field



Transport can be precisely controlled by scheduling the field



Electro-migration of charge carriers result in enhanced transport



Time Scales

$$\text{Diffusion time scale, } \tau_d = \frac{h^2}{D}$$

$$\text{Electrophoretic time scale, } \tau_E = \frac{h}{m q E_\infty}$$

Dimensionless Group

$$\text{Peclet No, } Pe_E = \frac{q h E_\infty}{k_B T} \sim 50 - 5000$$

Stokes-Einstein: $D = m k_B T$

Alvarez et al., PRE, 2010
Sengupta et al., PRE 2019

Conclusions

- Unstable suspensions yield accelerated, non-homogeneous breakup

Stable



Unstable



- Electro-migration of surfactant induced charge carriers result in ***precisely controlled, enhanced transport*** under electric fields

Acknowledgements

- NSF CBET-1066853, NSF CBET-1804548
- John E. Swearingen Fellowship, Carnegie Mellon University